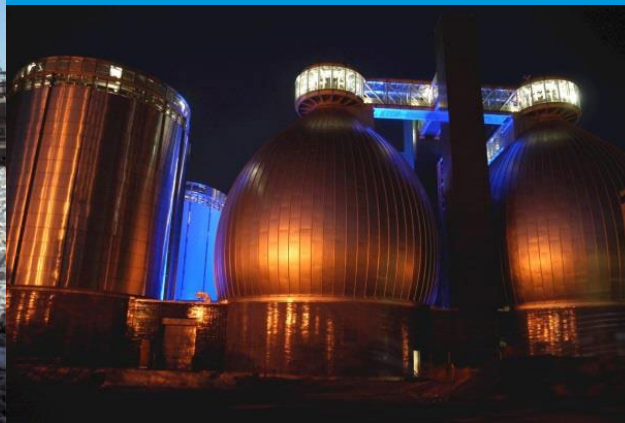


# Instrumentation Based Real-Time Process Optimization

November 13, 2018

Dave Rutowski  
Claros Process Optimization



# INSTRUMENTATION CONTINUUM

Passive (watch)

Active (control)

Do  
Nothing

Grab  
Samples

Online  
Analysis

Data:  
Aggregate  
Analyze  
Report

Decision  
Support:  
Detect  
Diagnose  
Predict

Control/  
Optimize  
Processes

Control/  
Optimize  
Facilities

SERVICE

Lab  
Equipment/  
Chemistries

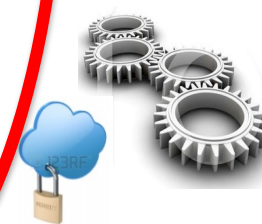
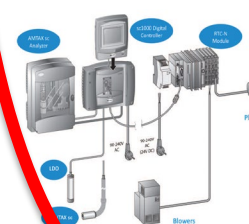
Process  
Equipment

WIMS

Prognosys/  
Sensor  
Verification

RTC

Claros



# LOTS OF VARIATIONS IN PROCESS CONTROL

## Operator Questions -

- What to measure – and why?
- Where to measure it?
- Is a daily grab sample representative, good enough?
  - **Hint: It is not**
- Is my plant running as designed?
- Is my instrument giving me correct readings?
- What do I do with the data?
- Do the chemical, power savings matter?
  - **Hint: Absolutely**

# UTILITY MARKET'S BUSINESS ISSUES

- Retiring workforce - Institutional knowledge is leaving the industry
- Grab sample process changes lead to chasing problems & never catching them
- Budget concerns
- Compliance regulations
- Data management



## Claros Overview

Instrument Management

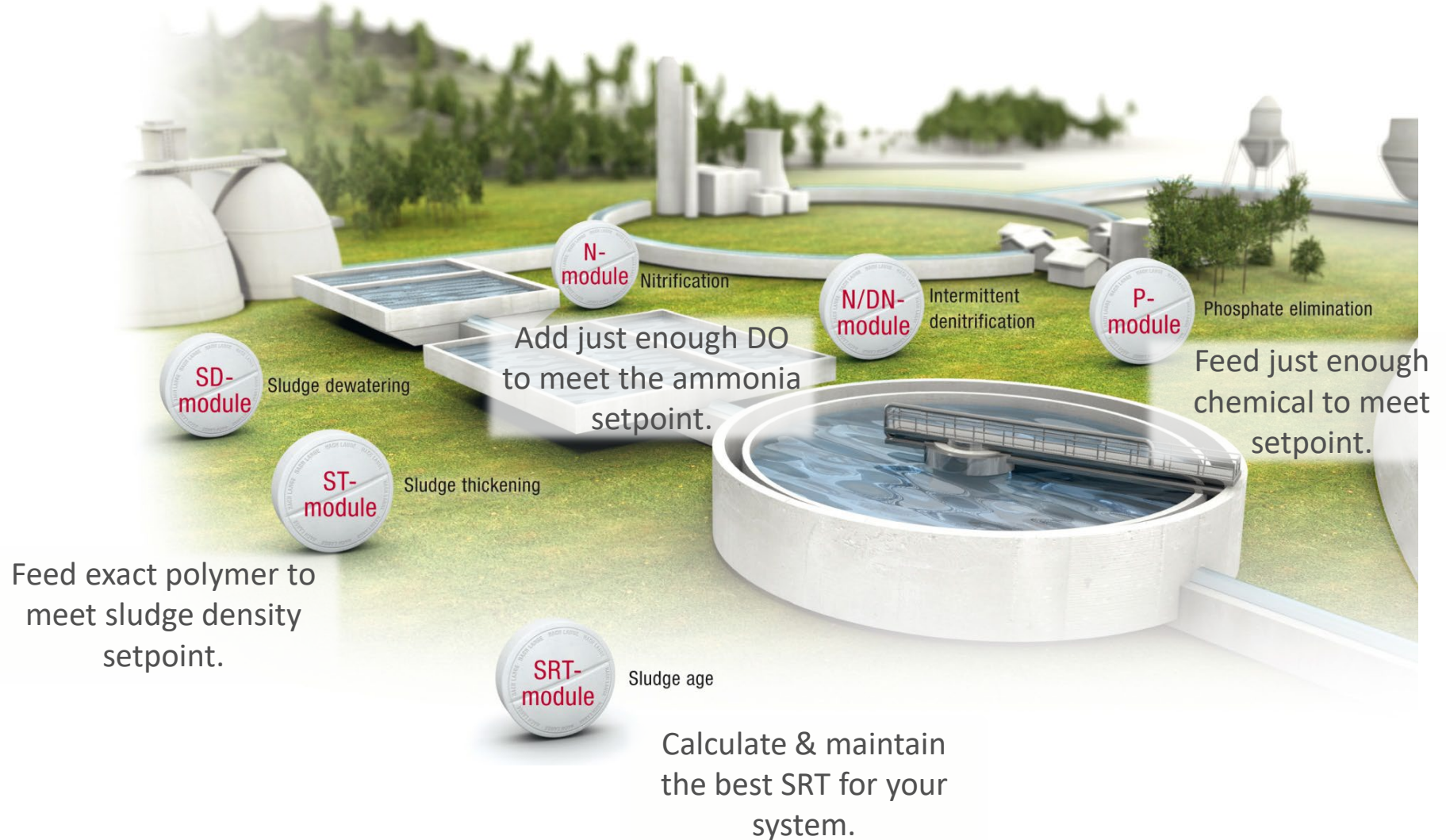
Data Management

Process Management

*Everyone is being asked to do more with less but how?*

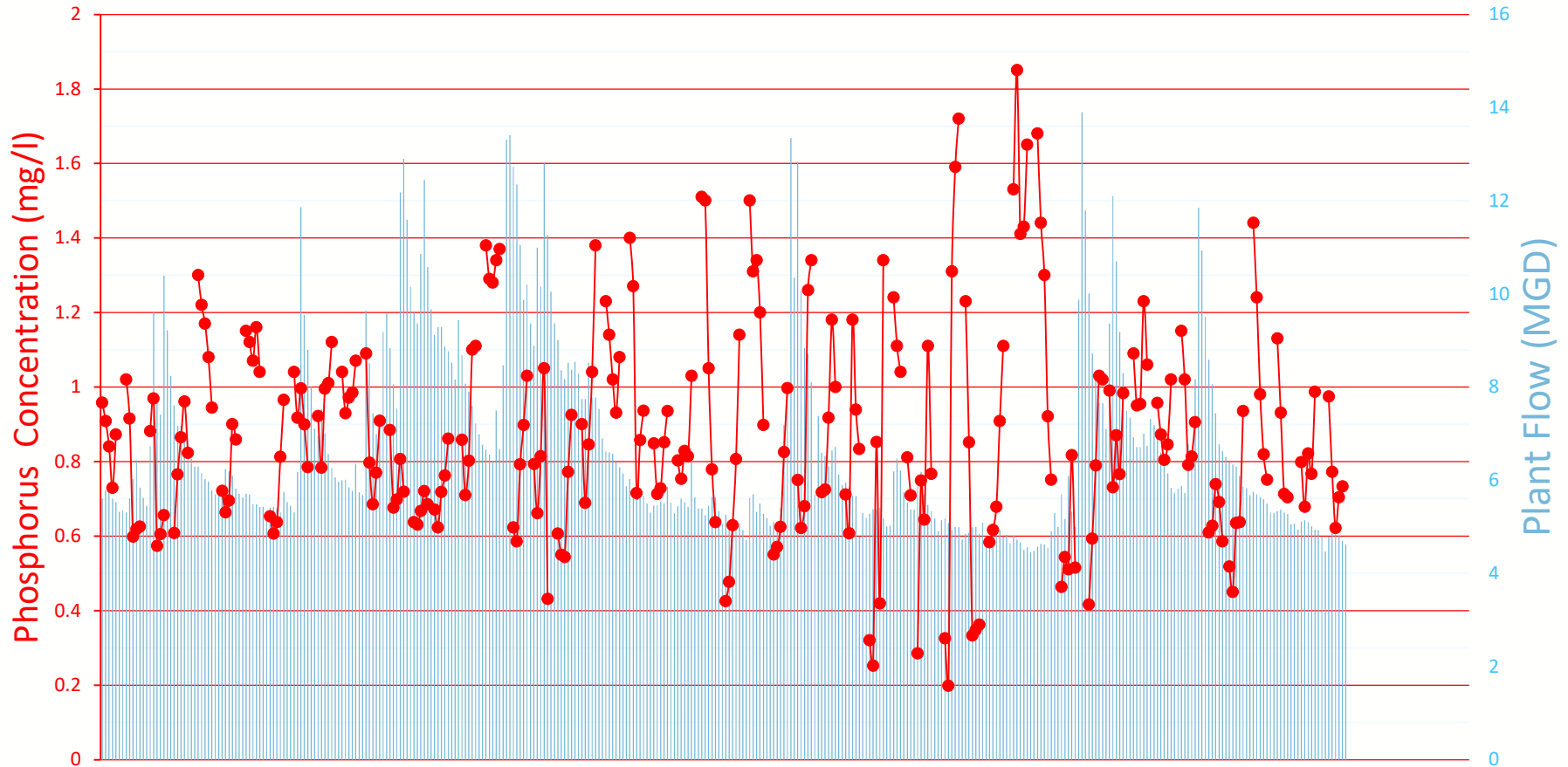


# RTC – REAL TIME CONTROL.



# ILLINOIS (CURRENT STATE)

Daily Flow / Phosphorus Concentration 2017



# ILLINOIS PHOSPHORUS LEVELS

Based on 2017 Data

146 days Spent overfeeding Alum

Cost:

22,552 gallons excess used (Actual vs. Target of 0.95 mg/l)

= 5 truckloads of Alum

**\$27,062**

# ILLINOIS PHOSPHORUS LEVELS

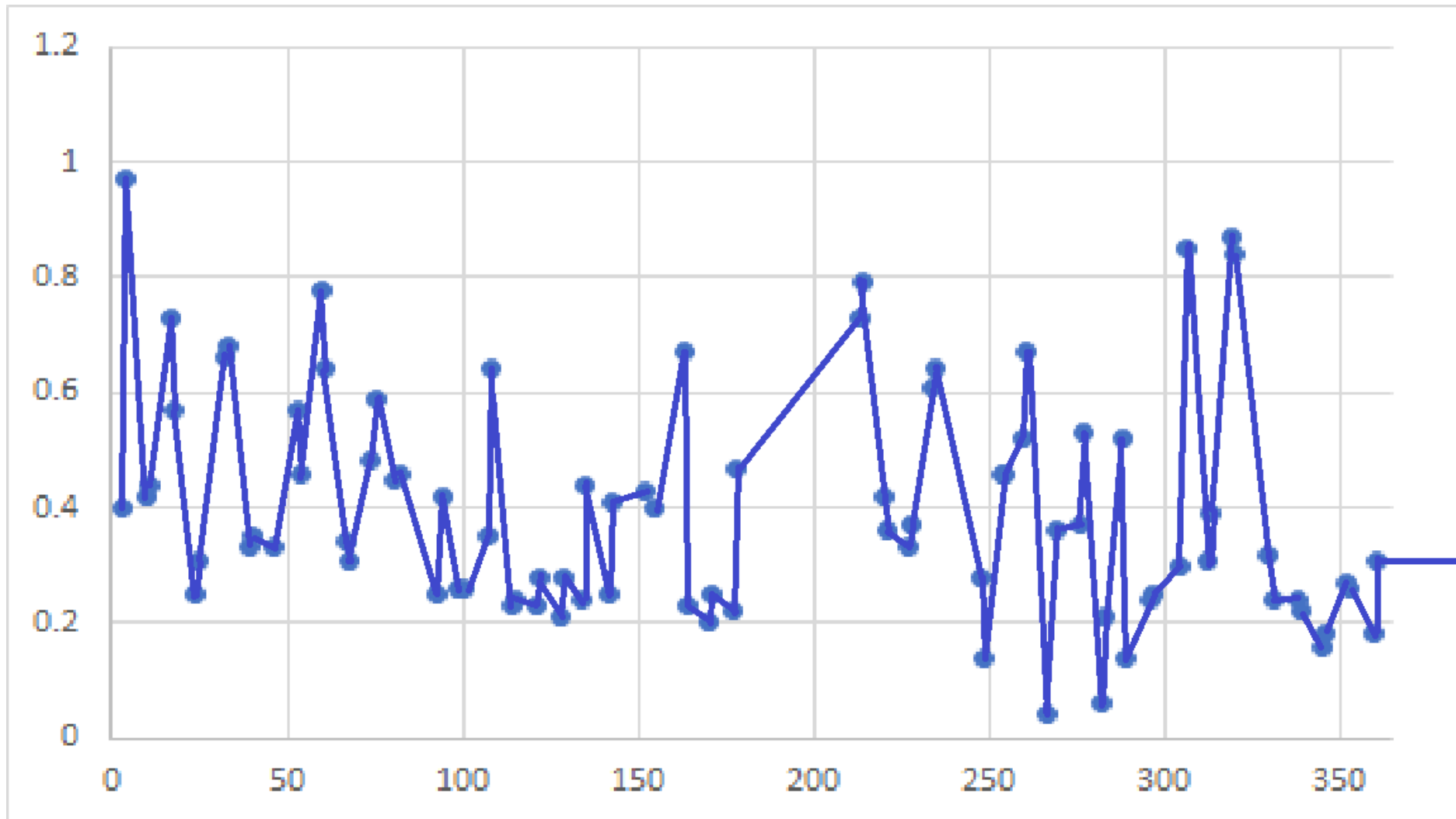
## DAILY COMPOSITE TESTING

Over 2.000	1	0.9-0.999	37	0.8-0.899	37
1.5-1.999	9			0.7-0.799	41
1.40-1.499	5			0.6-0.699	39
1.30-1.399	11			0.5-0.599	14
1.2-1.299	11			0.4-0.499	7
1.1-1.199	16			0.3-0.399	5
<u>1.0-1.099</u>	<u>24</u>			<u>Under 0.300</u>	<u>3</u>
	76		37		146

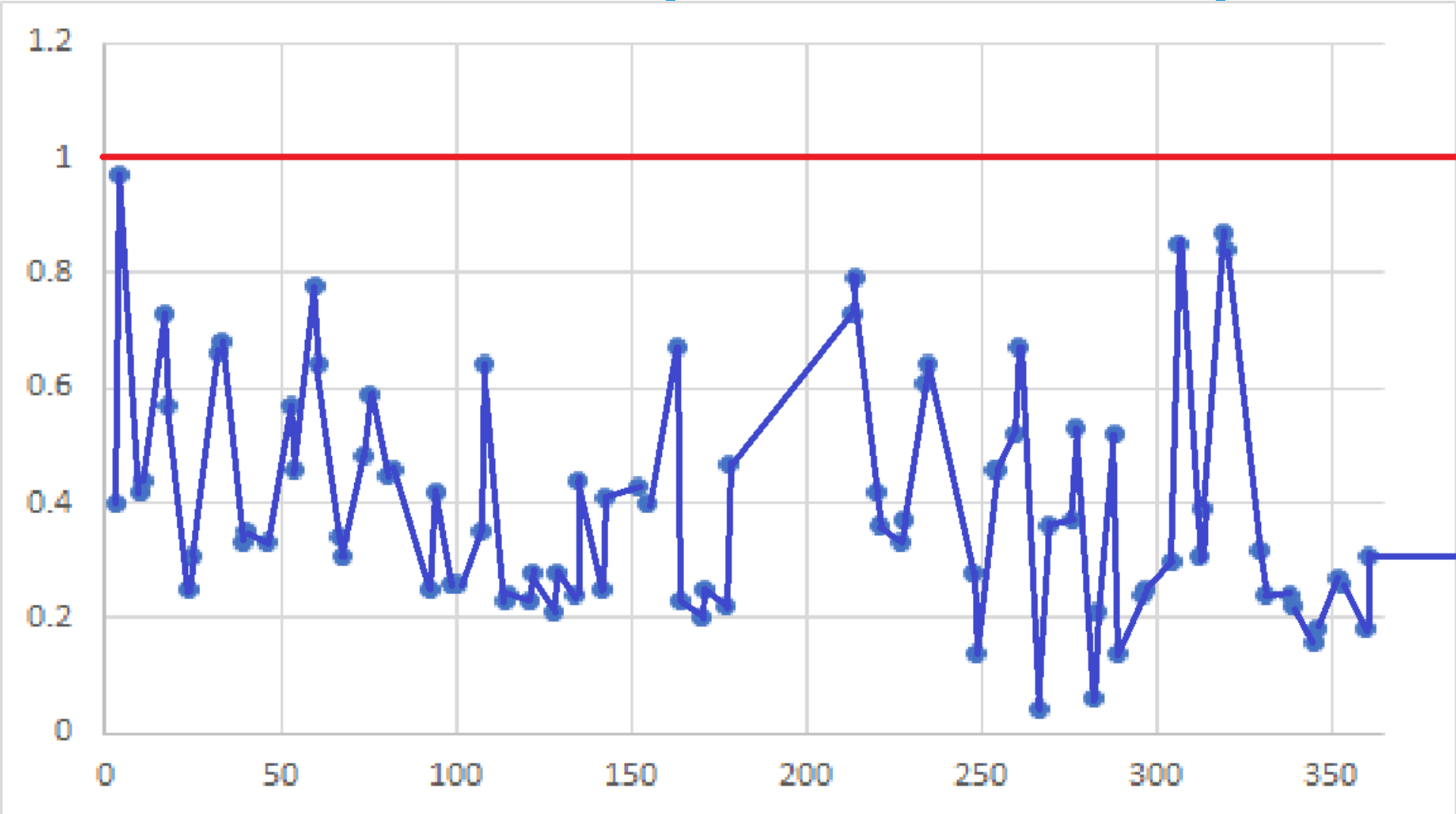
**NOT MONITORED 106**



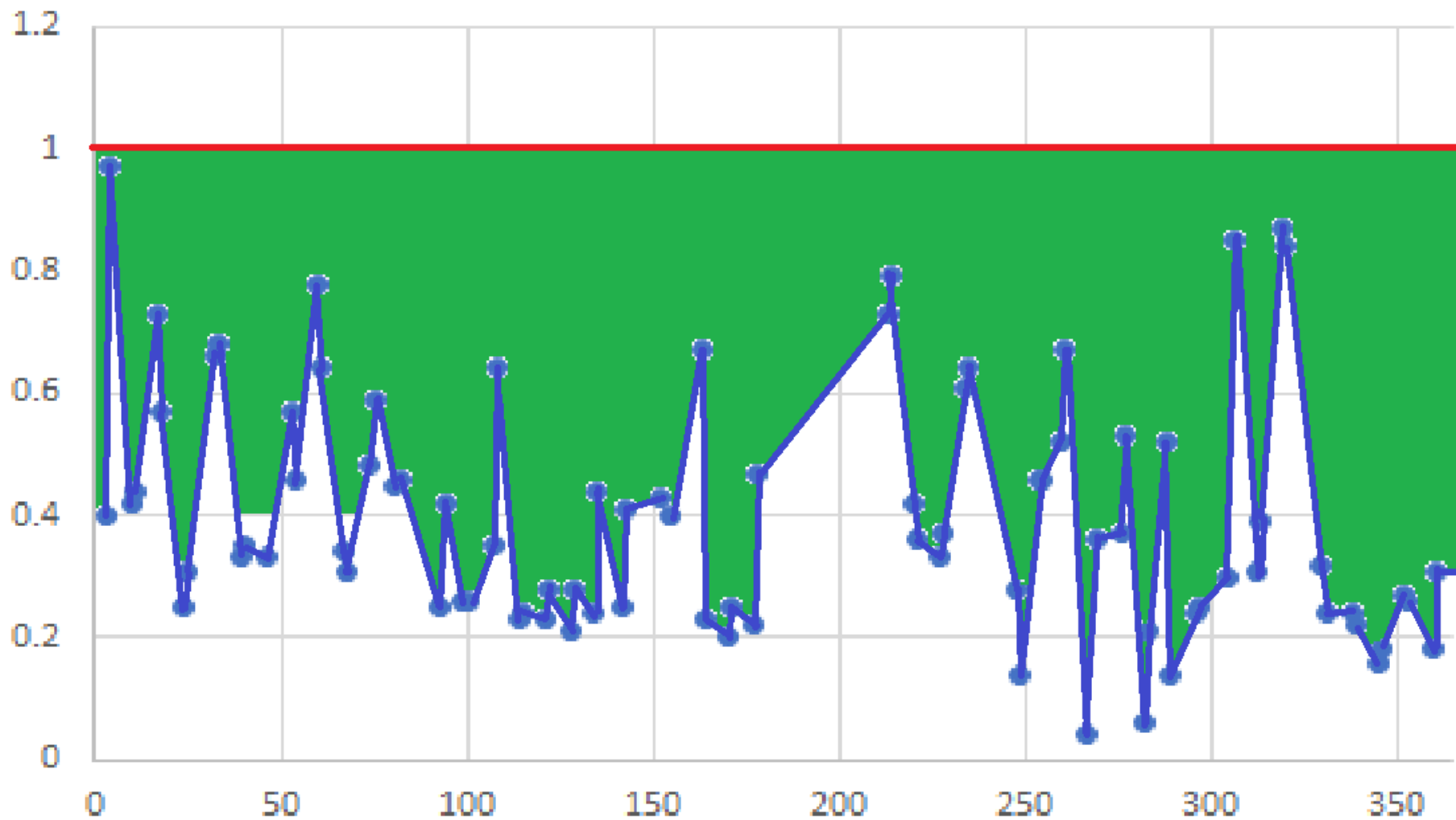
# OHIO WWTP (CURRENT STATE)



# OHIO WWTP (CURRENT STATE)



# OHIO WWTP (CURRENT STATE)



# OHIO WWTP PHOSPHORUS LEVELS

Based on 2017 Data:

Phosphorus Discharge permit limit = 1.0 mg/l

Average discharge = 0.40 mg/l

(87 days sampled in 2017)

Alum Overfeeding cost

(based on 0.95 mg/l target)

**\$78,999.60**

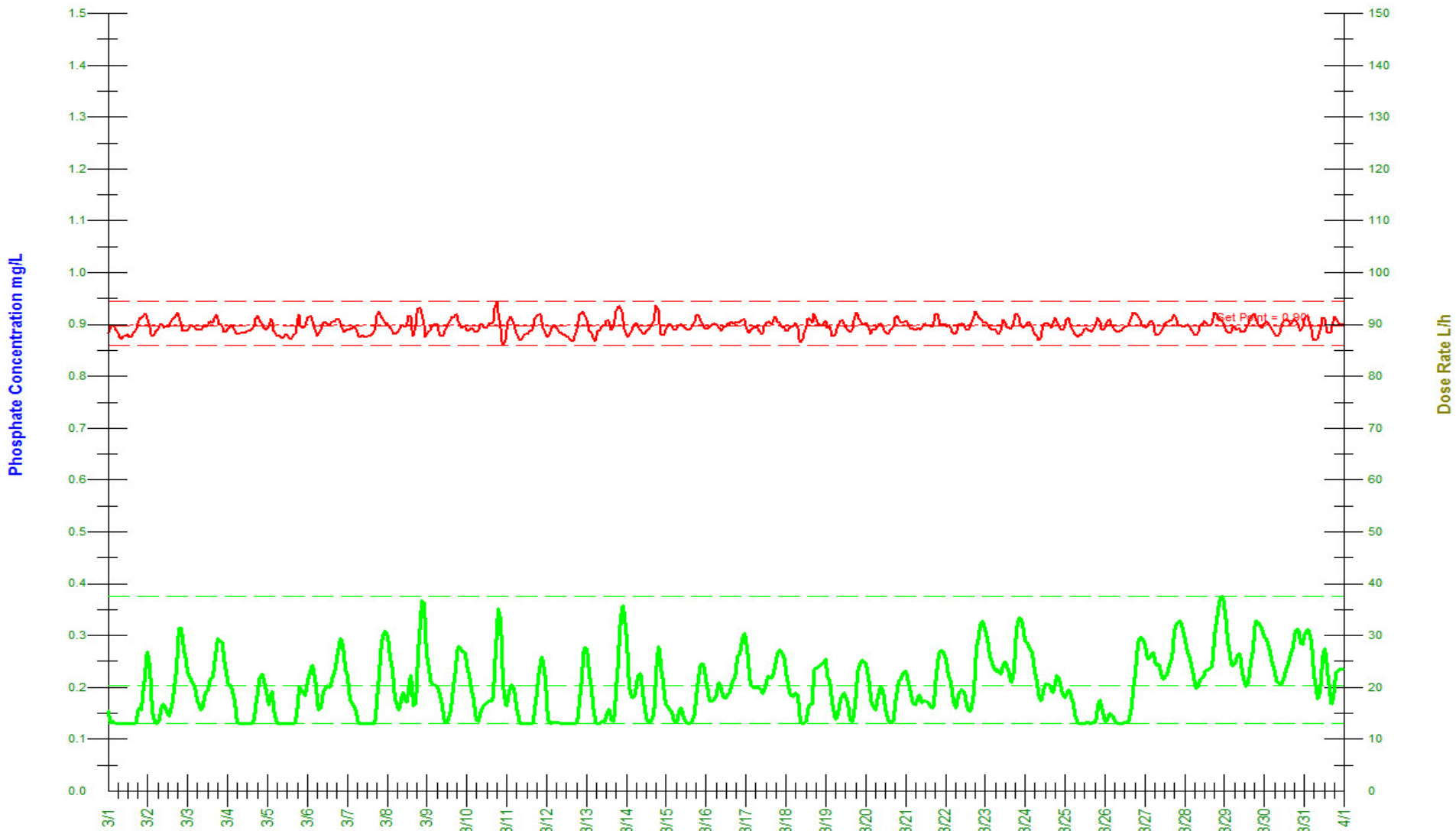
# Beaver Dam, WI

5.6 MGD (Design) Activated Sludge Plant

City of 16,000 residents



**Limit of 1.0 mg/L    Set point of 0.9 mg/L**  
**Never deviates outside of 0.85 – 0.95**





# Beaver Dam, WI

"If we were high one week, we overfed ferric to make sure the average for the month was below our 1.0 mg/L total phosphorus limit."

**The average dose was 300 gpd at 12.5 gph.**

Now during months of higher loading, the ferric feed rate may increase from **3 gph to 10 gph.**

"Estimated annual savings of \$50,000 to \$70,000 have more than paid for the system."

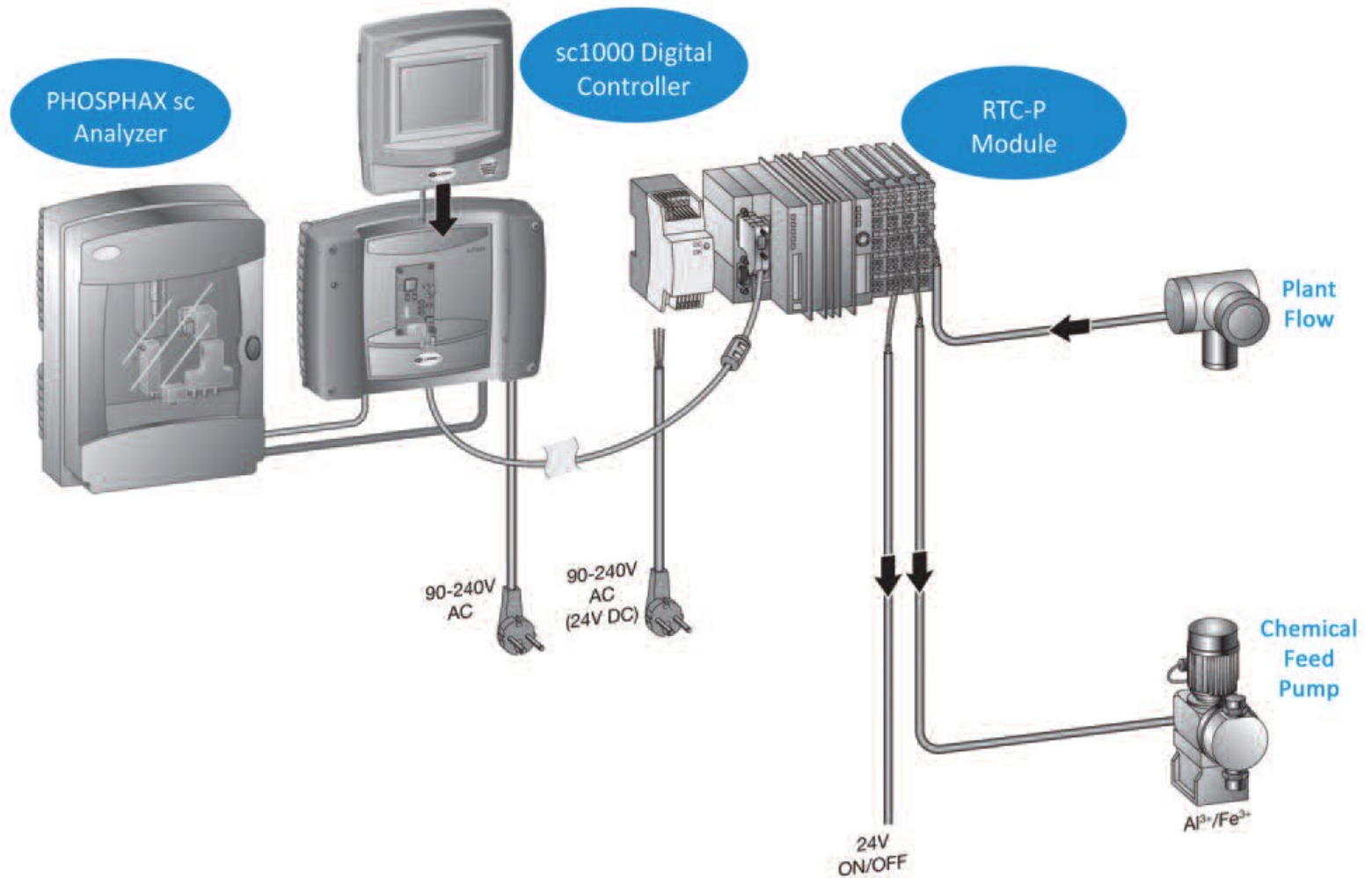
Besides affordability, a major benefit was ***peace of mind***. Previously, staff worried about whether the plant was over or at its limit for the month. "Now, the RTC controls the dose and I know we will be within our limit,"

"it has worked flawlessly."

**Rob Minnema**, *Director of Utilities Beaver Dam, WI*

# RTC1017P MODULE

## REAL TIME PHOSPHORUS CONTROL SOLUTION



# RTC-P

## Components



**PHOSPHAX sc +  
Filtrax**



### sc1000

- Controls RTC parameters
- Signal validation
- All communication capabilities



### RTC

- Calculates set-points in real time
- Interface for dosing pump
- Install in PLC cabinet



### Plant Flow

- Needed to determine loading

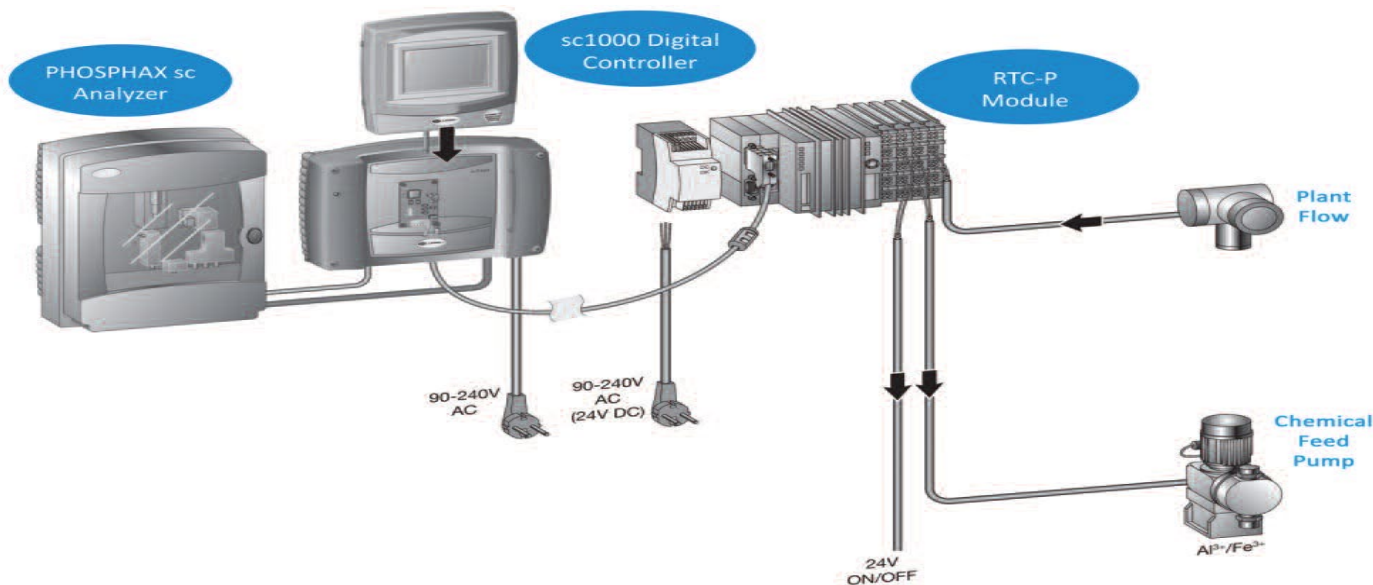


### Dosing Pump

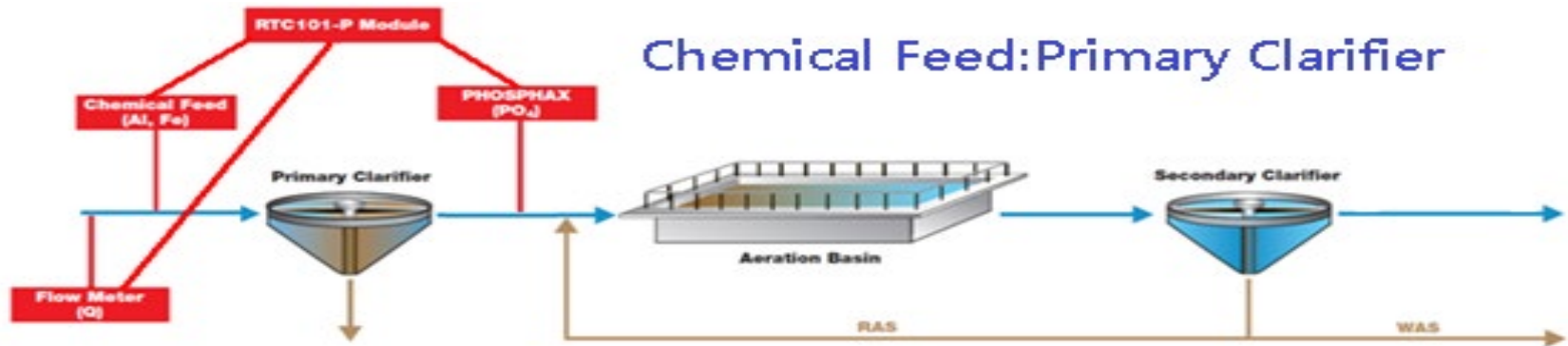
- Control pump feed of precipitant based on  $\text{PO}_4$  concentration

# WHY HACH'S RTC FOR PHOSPHORUS CONTROL?

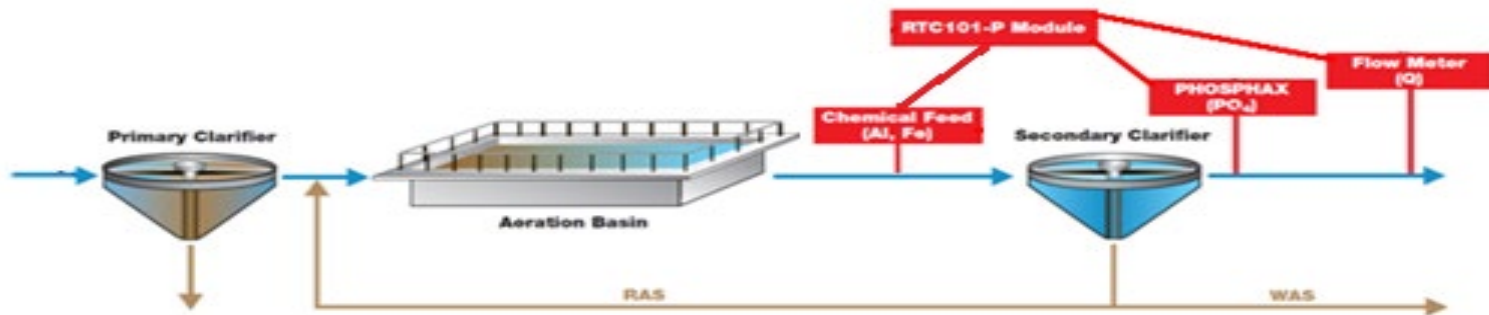
- Treatment Process is Optimized
  - Phosphorus load (Flow x Conc.) vs. Chemical effectiveness
- ROI is proven, can be switched between precipitants
- Cost savings can be redirected
- Compliance worries are gone
- Hach offers packaged integration!



# PO4-P PRECIPITANT CONTROL MODULE



## Chemical Feed: Secondary



# PHOSPHORUS ANALYZER– COLORMETRIC

- Sample Ranges
  - 0.0 – 2.0 mg/L PO<sub>4</sub>-P
  - 0.05 – 15.00 mg/L PO<sub>4</sub>-P
  - 1.0 – 50.00 mg/L PO<sub>4</sub>-P
- 5 – 120 minute measurement interval
  - Faster the interval...faster use of reagents

**Phosphax**





# SAMPLE CONDITIONING

## FILTRATION MODULES

- The Filtration Module prepares sample through two ultra-filtration membranes (0.15  $\mu$ )
- Modules are immersed in the process tank.
- Peristaltic pump pulls the sample through one filter at a time, allowing for optimal cleaning.
- Unit automatically cleans by forcing vigorous stream of air bubbles against sides of the filter modules.

**Filtrax sc**



# CONTROLLERS/TRANSMITTERS

## Standard Features

- Highly configurable
- Up To 8 Sensors
- Plug And Play Functionality
- C1D2 Certification
- NEMA 4x/Ip66
- 4 Relays
- Up To 12 Ma Outputs
- Up To 12 Ma Inputs
- SD Card For Data log And Configuration
- Networking
- Allows Up To 32 Devices Per Network

## Communication Options

- Modbus Rs232/Rs485
- Modbus TCP/IP
- Profibus Dp
- Hart 7.2

sc1000



# PHOSPHORUS DOSING CONTROL DESIGN QUESTIONS

- Model based or feedback?
- Control or modelling/trending?
- How much Chemical is required to remove the Phosphorus?
- Control the pumps directly, or have a separate SCADA control loop?
- What if something else is limiting reaction?
- How to integrate sensor diagnostics into the controls?
- Who will train everyone on the system?
- How long will it take to write and test the logic?
- What if a sensor fails?
- How to store the data?
- Who will write the O&M Manual?
- Who will fix it if it breaks?

# PHOSPHORUS DOSING CONTROL SOLUTIONS

## Hach RTC-P Module

- |  |                      |
|--|----------------------|
| 1. What to measure & where                   | ✓ Done               |
| 2. Can both model and/or control             | ✓ Done               |
| 3. Definition of control algorithms          | ✓ Done               |
| 4. Programming of control algorithms         | ✓ Done               |
| 5. Implementation on hardware                | ✓ Done               |
| 6. Testing of software and hardware          | ✓ Done               |
| 7. User interface                            | ✓ Done               |
| 8. User manual                               | ✓ Done               |
| 9. Backup stages                             | ✓ Done               |
| 10. Communications interface                 | ✓ Done               |
| 11. Data stored on IPC                       | ✓ Done               |
| 12. Onsite & remote support                  | ✓ Done               |
| 13. Setting of the plant-specific parameters | During commissioning |



*Be Right™*

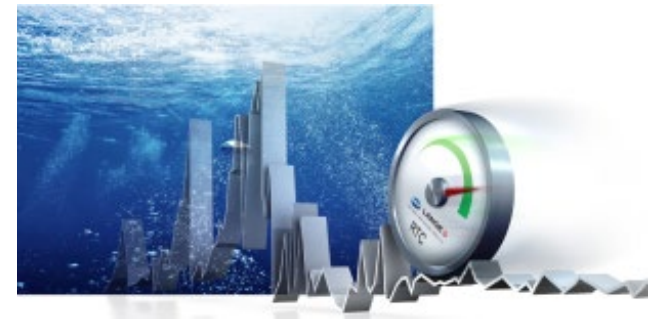
# CLAROS PROCESS MANAGEMENT



# PROCESS MANAGEMENT

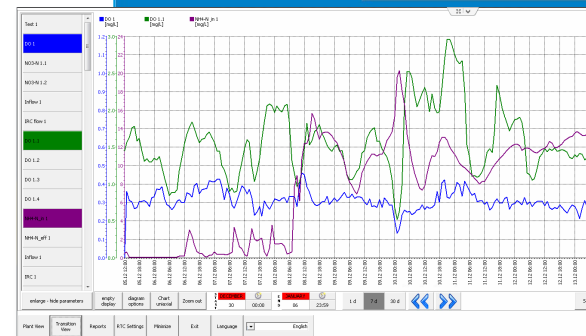
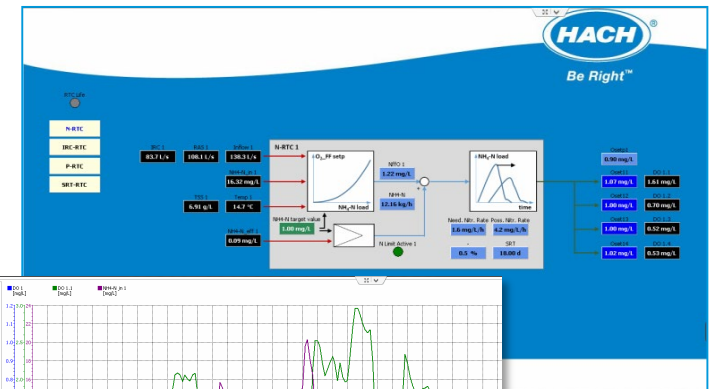
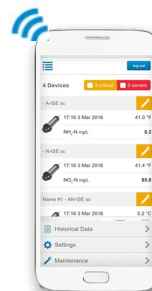
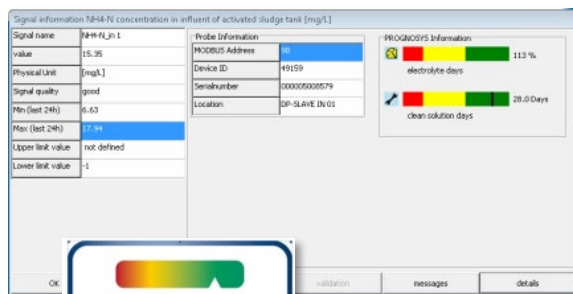
## Standardized RTC control modules

- Adapt asset plant operation to varying load situations and plant performance
  - Improved compliance (minimize risk)
  - Reduced OPEX / Short ROI (economically viable)
  - Improved process transparency



All analytical input signals **validated** by  
*Instrument Management* / PROGNOSYS®

- High reliability, high uptime



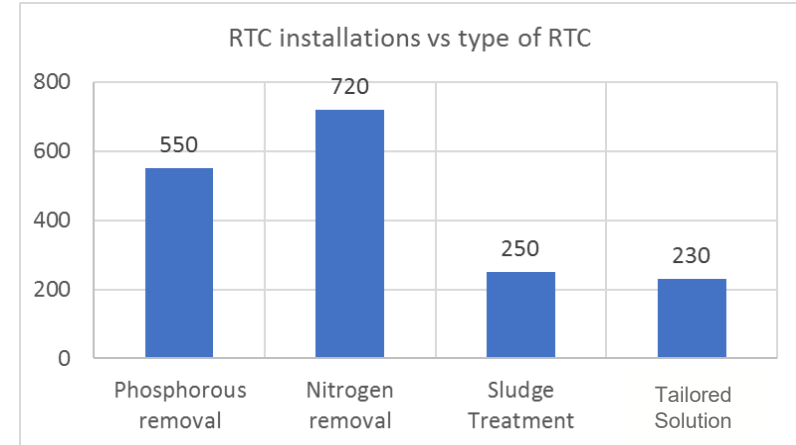




# PROCESS MANAGEMENT EXPERIENCE

## Large number of installations

- **1850 sites** in EU, US, China operating an RTC
  - 70 % of plants between 2-8 MGD
- **3150 control modules** in operation
- Growing number of industrial RTC



## Experienced Global RTC Team

- Growing team of RTC consultants
  - 28 in EU, 5 in US
- Sales & Service NA: 250 associates
- Centralized (US and EU) RTC Service/Commissioning experts providing remote support & monitoring



# PROCESS MANAGEMENT RTC MODULES

## Standardized modules for

- Nitrification / Denitrification
  - 10 - 20% aeration energy savings above conventional NH<sub>3</sub> trim optimization
  - Improved alkalinity
  - Reduced denitrification in Secondary Clarifiers
- Chemical phosphorous removal
  - Savings on precipitant (10 - 50%) and sludge disposal
  - Process stability by reducing loss in alkalinity
- Sludge treatment
  - Savings on polymer (15 - 20%)
  - Increased gas yield (5 - 10%)
  - Less sludge disposal cost (10 - 15%)
  - Reduced maintenance work



# REAL TIME CONTROL MODULES

Type	RTC	Application	Compliance	Direct Savings on
Nutrient Removal	P	Chemical P-elimination	$P_{tot}$	- Precipitant - Sludge treatment /disposal
	N	Nitrification (plug flow)	$NH_4-N$	- Energy (aeration <i>intensity</i> )
	DN	Denitrification (IRC / Ext. C)	$N_{tot}$	- Energy (DO recovery, <i>IRC</i> ) - External Carbon
	SZ	Swing zone adjustment	$N_{tot}$	- Energy (aerated <i>volume</i> )
	N/DN	Intermittent denitrification	$N_{tot}$ $NH_4-N$	- Energy (aeration <i>time/volume</i> , DO recovery)
	OXD	Simultaneous denitrification		
	DO	Aeration	$NH_4-N$	- Energy (controlled DO)
	SF	Nitrification (step feed)	$NH_4-N$	- Energy (aeration intensity)
	MOV	DO Control	NA	- Energy (aeration intensity)
Sludge Mgmt.	SRT	Sludge age	$NH_4-N$	- Energy (for BOD removal)
	ST	Sludge thickening		- Polymer, - Increased gas yield
	SD	Sludge dewatering		- Polymer - Sludge disposal
Industry	DOS	Nutrient dosing	$N_{tot}$ , $P_{tot}$ , $NH_4$	- Urea - Phosphoric acid
	DAF*1	Dissolved Air flotation	COD, TSS	- Coagulant, Polymer

**COMMITTED TO SUPPORT YOU  
FROM DESIGN TO OPERATION**

