

Lessons Learned -New Plant Start Up

Mark Chandler Operations Superintendent

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- Healthiest County in Ohio State Ranked #1 for last 4 years running
- Wealthiest County State Ranked #1 household median income
- Wisest
 50% of residents has bachelor degrees or higher
- 2nd Happiest County in U.S.
 Only behind Loudoun County, Virginia
- Fastest growing county in Ohio



Delaware County Regional Sewer District

- Alum Creek Water Reclamation Facility
- Olentangy Environmental Control Center
- Lower Scioto Water Reclamation Facility
- North Star Re-Use Facility
- Scioto Reserve Re-Use facility
- Tartan Fields Re-Use Facility
- Scioto Hills
- Hoover Woods
- Bent Tree



<u>Delaware County Regional</u> <u>Sewer District Operational Staff</u>





51 Operational Employees

- o 51 % is OEPA Certified
- o 25% is OWEA Lab Certified
- o 25% has college degrees
- o 80% has CDL







New Plants to Start Up in 2017

North Star Wastewater Re-Use Facility

- o Built by Developer starting 2007
- o Accepted by Delaware County 2008
- o Start Up Procedures started 2009

Lower Scioto Water Reclamation Facility

- Built by Developer- Delaware County 2009
- Accepted by Delaware County 2013
- Start Up Procedures started 2016





North Star Wastewater Re-Use Facility

- Construction completed 2009
- Service area includes 1695 acres
- 900 residential lots and 43 commercial lots
- Treatment Capacity of .500 MGD
- Zero discharge for golf course irrigation
- Operated under PTI recommended standards
- Regulated LAMP Permit 2013
- 55 million gallon storage impoundment
- 6 monitoring wells





North Star Wastewater Re-Use Facility Start Up Timeline

2009

- o Initial flow was estimated at less than 1000 gpd
- o Hired contractor to haul from pump station in lieu of treating
- Eventually pump station turned on to pump to plant
- Operator maintaining and exercising equipment
- No discharge to impoundment
- Economy crashed, no development

- o Pump station on pumping to plant
- o Minimal flows, holding flow at plant, providing minimal treatment
- Operating under PTI recommendations, no effluent limits
- Treating flow at plant in batches
- Operator maintaining and exercising equipment
- Discharged May and June

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- o Discharged January and April

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- Operating under PTI recommendations, no effluent limits
- Treating flow at plant in batches
- Operator maintaining and exercising equipment
- Discharged April, July, September, November, December

 $\circ~$ Pump station on pumping to plant

- Minimal flows, holding flow at plant, providing minimal treatment
- o Operating under New LAMP permit, effluent limits required
- o Treating flow at plant in batches
- o Pre-fab aeration tanks starting to fail
- o Operator maintaining and exercising equipment
- o Discharged April, May, June, July,

- o Pump station on pumping to plant
- o Minimal flows, holding flow at plant, providing minimal treatment
- o Operating under New LAMP permit, effluent limits required
- o Treating flow at plant in batches
- o Pre-fab tanks being repaired
- o Moratorium placed on developer to stop building
- o Operator maintaining and exercising equipment
- o Discharged March

- o Operations stopped
- Pump station off, contractor hauling flow from pump station
- o Pre-fab tanks being repaired
- o Moratorium still in place
- No discharge from plant

- o Pre-fab tank repairs complete
- o Moratorium lifted
- Pump Station back on pumping to plant in December
- Operating under New LAMP permit, effluent limits required
- o Discharged in December





- Pump Station in auto pumping to plant
- Operating under New LAMP permit
- Rough start with TIN compliance due to tank testing, no RAS pumping, Calcium Nitrate Ca(NO3)2 from pump station and road closure
- Operational learning curve, mainly with large bubble mixing-high D.O concentrations in anoxic zones
- Average daily flows 0.0302 MGD
- o 1st half 2017 average TIN 39.47 mg/l
- o 2nd half 2017 average TIN 6.0 mg/l mg/l



- $\,\circ\,$ Average TIN $\,$ 3.75 mg/l to date $\,$
- o Operators maintaining building and grounds
- Operators learning and optimizing treatment processes
- o Development growing in service area
- $\,\circ\,$ Average daily flows to date 0.0084 MGD



Start Up Strategy

1-Select existing tankage to be used for low flow start up, minimal tankage available to be compatible with start up flow, 1 anoxic tank and 1 aeration to be used.

2-Fill tanks with impoundment water

3-Build solids inventory by hauling in sludge from other plants to start nitrification process

4- Optimize anoxic zone by large bubble mixing and use of carbon feed system

5- Set up aeration blower on-off schedule to support the denitrification process

6-Treatment Steps, 1st Nitrification, 2nd Denitrification and 3rd Nutrient Removal

7- Process Control Targets:

MLSS- 2500 mg/l (2.5 spin) NH3- < 1.0 mg/l NO3- < 5.0 mg/l 30 minute SSV- 800-5 minutes, 400-30 minutes

8- LAMP permit effluent parameters: CBOD-40 mg/l TSS-45 mg/l TIN-10 mg/l E coli- 126- #100 ml

Start Up Challenges

- o Low flows
- o Structure failure
- o Equipment failure
- o Equipment warranties expired
- o New LAMP permit issued 2013
- o Trying to treat while testing tanks
- o Trying to denitrify with no RAS pumping
- o Tank freezing due to low flow
- o Broken non-pot lines, RAS lines
- o County Road to plant out of service for several months
- o Calcium Nitrate Ca(NO3)2 in force main to much for plant
- o Calcium Nitrate turned off, Force Main goes septic









Lower Scioto Water Reclamation Facility



- Screening
- Anoxic Zones
- Aeration
- Clarification
- Tertiary Filtration
- Aerobic Digestion
- UV Disinfection
- Centrifuge

Lower Scioto Water Reclamation Facility Start Up Timeline

2009

- o Construction complete
- Economy crashed, no development, no collection system
- o County employees attended over 150 hours manufacturer start up training
- Spare parts received, equipment inventory conducted

- o Plant sits idle, no operational activity
- No development, no collection system, no pipes in or out
- Developer responsible for maintaining plant
- o Contractor exercising equipment



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- Influent/Effluent line from plant to O'Shaughnessy P.S project started

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- o No development , No collection system
- o Developer responsible for maintaining plant
- o No exercising equipment
- Influent/Effluent line from plant to O'Shaughnessy P.S project completed





- o County assumes developer debt, takes full ownership and responsibility of plant
- Operations Manager and Package Plant Staff moves into Admin Building in October
- o Operators starts maintaining building and grounds
- Staff begins evaluations of design, tanks and valving configurations

2014

- o Operators maintaining buildings and grounds
- o Reviewing design prints for tank valving configurations

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- Reviewing design prints for tank valving configurations
- Start planning operational strategy
- o O'Shaughnessy Pump Station nears completion



- o Operators maintaining buildings and grounds
- Reviewing design prints for tank valving configurations
- Planning operational strategy
- o Testing new pump station and force main
- Exercising/Testing equipment and making repairs



- o 30 day hydraulic testing began in July to determine functionality of plant
- Water from O'Shaughnessy reservoir was pumped into new pump station and then on to plant
- Results from testing was used to create plan of action to address issues before start up of plant
- On November 13th flow was diverted from the Clear Creek pump station at 10:27am to the O'Shaughnessy pump station and at 12:01pm flow made it to the plant

Flow Arrives to Plant November 13th 12:01 pm





- o Operators maintaining plant
- o Development slowly starting
- Average daily flows to date 0.089 MGD
- o Average effluent TN 3.9 mg/l to date
- o Average TP 0.19 mg/l to date







Start Up Strategy

1- Select existing tankage to be used for low flow start up, minimal tankage available to be compatible with start up flow, 3 designed anoxic tanks with 1 being for aeration was used.

2-Fill tanks with ground/river water

3- Build solids inventory by hauling in sludge from other plants to start nitrification process

4- Optimize anoxic zone by large bubble mixing

5- Set up aeration blower on-off schedule to support the denitrification process

6-Treatment Steps, 1st Nitrification, 2nd Denitrification and 3rd Nutrient Removal

7- Process Control Targets:

MLSS- 2500 mg/l (2.5 spins) NH3- < 1.0 mg/l TN- < 10.0 mg/l 30 minute SSV- 800-5 minutes, 400-30 minutes

8- NPDES permit weekly effluent parameters: CBOD-5 mg/l TSS-18 mg/l TN-10 mg/l TP- 1.5 mg/l E coli- 284- #100 ml

Start Up Challenges

- o Low flows
- o Low effluent discharge limits
- General equipment failure, pumps, actuators, level sensors, plc's, SCADA, etc.
- o Equipment warranties expired
- o Equipment breakdown
- o Air release valve on the force main was leaking
- Ferric Chloride pumps and did not work properly, broken pipes and valves
- A non pot line above main feeder breaker and generator froze and busted damaging all surge protection and caused a power outage for about 24 hours





Lessons Learned

- Don't build a wastewater plant during an economic crisis
- Make sure plant design includes tanks, blowers and pumps to accommodate low flow start up periods
- o Evaluate pre-fab tanks vs. poured concrete walls
- $\,\circ\,$ Do not underestimate the solids inventory needed for start up
- o Provide treatment one step at a time, nitrification, denitrification and nutrient removal
- Follow process control methods to evaluate environments
- o Make sure all equipment valves are functioning before flow arrives
- Set up manufacturer start up training, review O&M manuals
- Try to trust SCADA, but do so cautiously
- Be prepared for Murphy's Law to apply "Anything that can go wrong will go wrong".

Questions ?

